

**AMENDMENTS TO THE CLAIMS:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**LISTING OF CLAIMS:**

1-16 (Cancelled)

17. (New) A process for manufacturing acrylic acid from propane, wherein:

- a) a gaseous mixture devoid of molecular oxygen and comprising propane, water vapour, as well as, if appropriate, an inert gas, is introduced into a first reactor with a moving catalyst bed,
- b) at the outlet of the first reactor, the gases are separated from the catalyst;
- c) the catalyst is returned into a regenerator;
- d) the gases are introduced into a second reactor with a moving catalyst bed;
- e) at the outlet of the second reactor, the gases are separated from the catalyst and the acrylic acid contained in the separated gases is recovered;
- f) the catalyst is returned into the regenerator;
- g) the regenerated catalyst from the regenerator is reintroduced into the first and second reactors;

and wherein the catalyst comprises molybdenum, vanadium, tellurium or antimony, oxygen and at least one other element X chosen from niobium, tantalum, tungsten, titanium, aluminium, zirconium, chromium, manganese, iron, ruthenium, cobalt, rhodium, nickel, palladium, platinum, antimony, bismuth, boron, indium and cerium.

18. (New) A process according to claim 17, wherein the first and second reactors are vertical and the catalyst is moved upwards by the gas flow.

19. (New) A process according to claim 17, wherein the temperature of the reactors is comprised between 200 to 500°C.

20. (New) A process according to claim 17, wherein the temperature of the reactors is comprised between 250 to 450°C.

21. (New) A process according to claim 17, wherein the pressure in the reactors is comprised between  $1.01 \times 10^4$  and  $1.01 \times 10^6$  Pa (0.1 to 10 atmospheres).

22. (New) A process according to claim 17, wherein the pressure in the reactors is comprised between  $5.05 \times 10^4$  and  $5.05 \times 10^5$  Pa (0.5-5 atmospheres).

23. (New) A process according to claim 17, wherein the residence time of the gases in each reactor is comprised between 0.01 and 90 seconds.

24. (New) A process according to claim 17, wherein the residence time of the gases in each reactor is comprised between 0.1 and 30 seconds.

25. (New) A process according to claim 17, wherein the regeneration of the catalyst is carried out by heating in the presence of oxygen or a gas containing oxygen, at a temperature of 250 to 500°C.

26. (New) A process according to claim 17, wherein the propylene produced originating from the gases separated in stage e) or the propane which has not reacted or both are recycled to the inlet of the reactor.

27. (New) A process according to claim 17, wherein the proportions of the elements of the catalyst meet the following conditions:

$$0.25 < r_{\text{Mo}} < 0.98$$

$$0.003 < r_{\text{V}} < 0.5$$

$$0,003 < r_{\text{Te}} \text{ or } r_{\text{Sb}} < 0.5$$

$$0.003 < r_{\text{X}} < 0.5$$

wherein  $r_{\text{Mo}}$ ,  $r_{\text{V}}$ ,  $r_{\text{Te}}$  and  $r_{\text{X}}$  represent the mole fractions, respectively, of Mo, V, Te and X, in relation to the sum of the numbers of moles of all the elements of the catalyst, with the exception of oxygen.

28. (New) A process according to claim 17, wherein the catalyst corresponds to formula (I) or to formula (Ia) below:



wherein:

- a) a is comprised between 0.006 and 1, inclusive;
- b) b is comprised between 0.006 and 1, inclusive;
- c) c is comprised between 0.006 and 1, inclusive;
- d) d is comprised between 0 and 3.5, inclusive; and

- e) x is the quantity of oxygen bound to the other elements and depends on their oxidation states.

29. (New) A process according to claim 28, wherein, in formula (I) or (Ia):

- a is comprised between 0.09 and 0.8, inclusive;
- b is comprised between 0.04 and 0.6, inclusive;
- c is comprised between 0.01 and 0.4, inclusive; and
- d is comprised between 0.4 and 1.6, inclusive.

30. (New) A process according to claim 17, wherein, at least one of the two reactors comprises a cocatalyst corresponding to the following formula (II):



wherein:

- a' is comprised between 0.006 and 1, inclusive
- b' is comprised between 0 and 3.5, inclusive;
- c' is comprised between 0 and 3.5, inclusive;
- d' is comprised between 0 and 3.5, inclusive;
- e' is comprised between 0 and 1, inclusive;
- f' is comprised between 0 and 1, inclusive;
- g' is comprised between 0 and 1, inclusive;
- h' is comprised between 0 and 3.5, inclusive;
- i' is comprised between 0 and 1, inclusive;
- j' is comprised between 0 and 1, inclusive;
- k' is comprised between 0 and 1, inclusive;
- l' is comprised between 0 and 1, inclusive;
- m' is comprised between 0 and 1, inclusive; and
- n' is comprised between 0 and 1, inclusive.

31. (New) A process according to claim 30 wherein the cocatalyst is regenerated and circulates in the same way as the catalyst.

32. (New) A process according to claim 30, wherein, in the cocatalyst of formula(II):

- a' is comprised between 0.01 and 0.4, inclusive;
- b' is comprised between 0.2 and 1.6, inclusive;
- c' is comprised between 0.3 and 1.6, inclusive;

- d' is comprised between 0.1 and 0.6, inclusive;
- e' is comprised between 0.006 and 0.01, inclusive;
- f' is comprised between 0 and 0.4, inclusive;
- g' is comprised between 0 and 0.4, inclusive;
- h' is comprised between 0.01 and 1.6, inclusive
- i' is comprised between 0 and 0.4, inclusive;
- j' is comprised between 0 and 0.4, inclusive;
- k' is comprised between 0 and 0.4, inclusive;
- l' is comprised between 0 and 0.4, inclusive;
- m' is comprised between 0 and 0.4, inclusive; and
- n' is comprised between 0 and 0.4, inclusive.

33. (New) A process according to claim 30, wherein, a weight ratio of the catalyst to the cocatalyst greater than 0.5 is used.

34. (New) A process according to claim 30, wherein, a weight ratio of the catalyst to the cocatalyst of at least 1 is used.

35. (New) A process according to claim 30, wherein the catalyst and the cocatalyst are mixed.

36. (New) A process according to claim 30, wherein the catalyst and the cocatalyst are present in the form of pellets, each pellet comprising both the catalyst and the cocatalyst.

37. (New) A process for manufacturing acrylic acid from propane, wherein:

- a) a gaseous mixture devoid of molecular oxygen and comprising propane, water vapour, as well as, if appropriate, an inert gas, is introduced into a first reactor with a moving catalyst bed,
- b) at the outlet of the first reactor, the gases are separated from the catalyst;
- c) the catalyst is returned into a regenerator;
- d) the gases are introduced into a second reactor with a moving catalyst bed;
- e) at the outlet of the second reactor, the gases are separated from the catalyst and the acrylic acid contained in the separated gases is recovered;
- f) the catalyst is returned into the regenerator;

g) the regenerated catalyst from the regenerator is reintroduced into the first and second reactors;

and wherein:

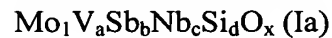
the first and second reactors are vertical and the catalyst is moved upwards by the gas flow;

the temperature of the reactors is comprised between 250 to 450°C;

the pressure in the reactors is comprised between  $5.05 \times 10^4$  and  $5.05 \times 10^5$  Pa (0.5-5 atmospheres);

the residence time of the gases in each reactor is comprised between 0.1 and 30 seconds;

the catalyst corresponds to formula (I) or to formula (Ia) below:



wherein:

h) a is comprised between 0.006 and 1, inclusive;

i) b is comprised between 0.006 and 1, inclusive;

j) c is comprised between 0.006 and 1, inclusive;

k) d is comprised between 0 and 3.5, inclusive; and

l) x is the quantity of oxygen bound to the other elements and depends on their oxidation states.

38. (New) A process for manufacturing according to claim 33, wherein, in formula (I) or (Ia):

- a is comprised between 0.09 and 0.8, inclusive;
- b is comprised between 0.04 and 0.6, inclusive;
- c is comprised between 0.01 and 0.4, inclusive; and
- d is comprised between 0.4 and 1.6, inclusive.

39. (New) A process according to claim 33, wherein the propylene produced originating from the gases separated in stage e) or the propane which has not reacted or both are recycled to the inlet of the reactor.

40. (New) A process according to claim 33, wherein, at least one of the two reactors comprises a cocatalyst corresponding to the following formula (II):



wherein:

- a' is comprised between 0.006 and 1, inclusive
- b' is comprised between 0 and 3.5, inclusive;

- c' is comprised between 0 and 3.5, inclusive;
- d' is comprised between 0 and 3.5, inclusive;
- e' is comprised between 0 and 1, inclusive;
- f' is comprised between 0 and 1, inclusive;
- g' is comprised between 0 and 1, inclusive;
- h' is comprised between 0 and 3.5, inclusive;
- i' is comprised between 0 and 1, inclusive;
- j' is comprised between 0 and 1, inclusive;
- k' is comprised between 0 and 1, inclusive;
- l' is comprised between 0 and 1, inclusive;
- m' is comprised between 0 and 1, inclusive; and
- n' is comprised between 0 and 1, inclusive.